

# **An Environmentally Friendly Closed-Loop Geothermal Energy Extraction System**

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# Introduction

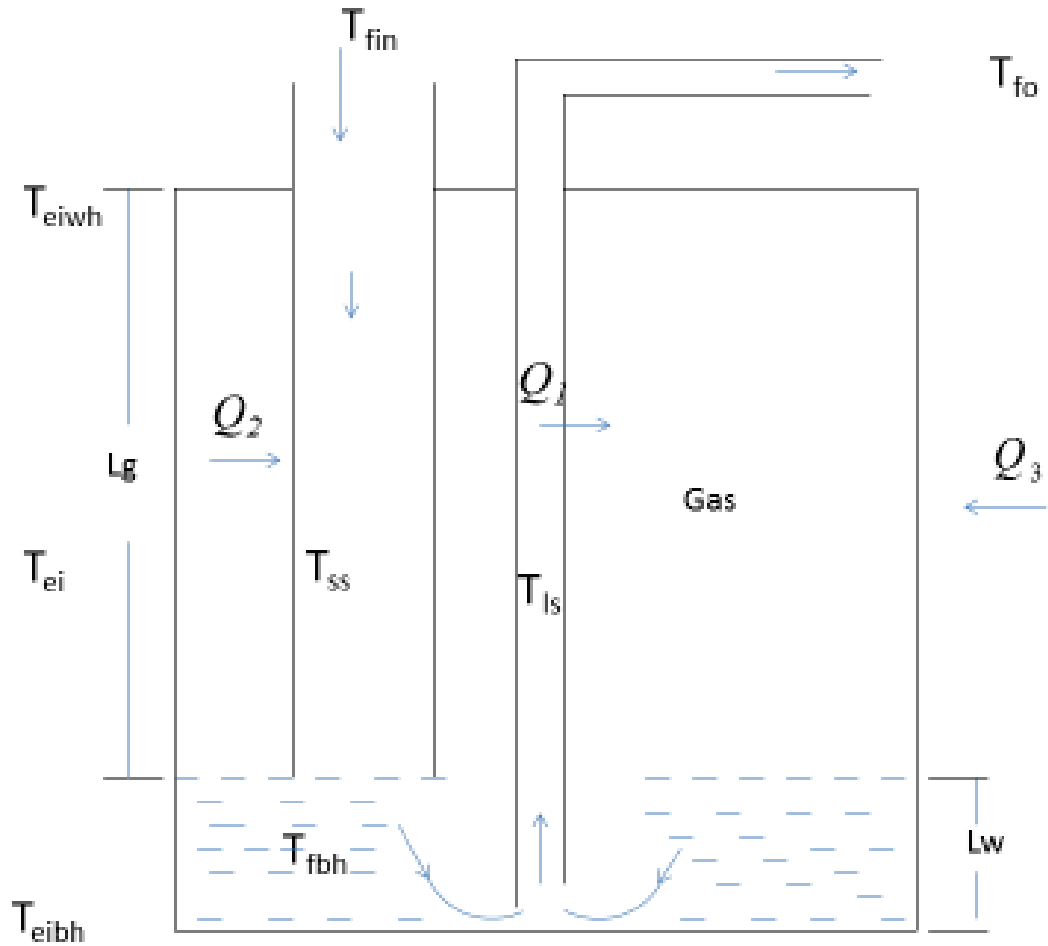
- Most geothermal power plants use hot water/steam sources; producing from dry rock require water injection
- Our closed loop model uses production and injection tubing
- Water doesn't invade the rock
- Formation isn't contaminated



# Model description

- Production and Injection tubing
- Nitrogen Gas blanket
- Long string for production
- Short string for injection
- Water injection rate same as production rate





$$Q_2 = Q_1 + Q_3$$

$L_g$  = height of the wellbore above the water level

$L_w$  = height of water

ls = long string

ss = short string

Fig: Schematic of the wellbore



# Theory

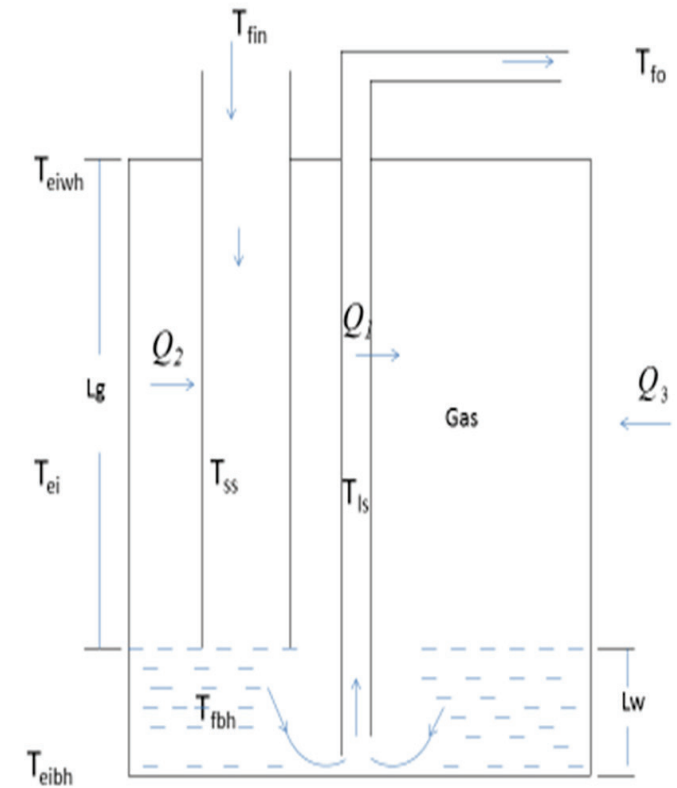
Wellbore has two sections

Top ← GS (Gas Section)

Bottom → LS (Liquid section)

Surrounding formation exchanges heat with the annulus:

$$Q_3 = w c_p L_R (T_{ei} - T_a)$$



# Gas Section:

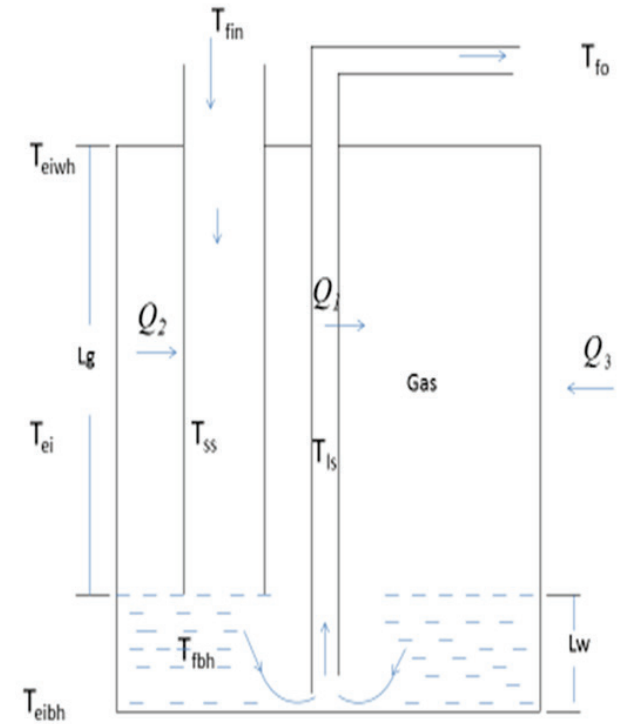
Prod. string exchange heat with annulus:

$$Q_1 = 2\pi r_{ls} U_{ls} (T_{ls} - T_a)$$

Injection string heat from gas in annulus:

$$Q_2 = 2\pi r_{ss} U_{ss} (T_a - T_{ss})$$

U = Overall heat transfer coefficient



## Liquid Section:

- Fluid in the tubing moving up
- Annulus fluid moving downward
- Heat exchange between the annulus and the fluid:

$$Q_{ta} = 2\pi r_{ls} U_{ta} (T_a - T_{ls})$$

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# Governing Eq.

$$c_{pa} \frac{dT_a}{dz} + D_a = L_{R2} c_{pa} (T_{ei} - T_a) + \frac{c_{pa}}{B} (T_t - T_a)$$

$$\frac{dT_{ls}}{dz} = (T_{ls} - T_a) \frac{2\pi r_{ls} U_{ls}}{c_{pls} w_{ls}} - \frac{g \sin \theta_G}{c_{pls}} + \phi_{ls}$$

$$\frac{dT_{ss}}{dz} = (T_a - T_{ss}) \frac{2\pi r_{ss} U_{ss}}{c_{pss} w_{ss}} - \frac{g \sin \theta_G}{c_{pss}} + \phi_{ss}$$

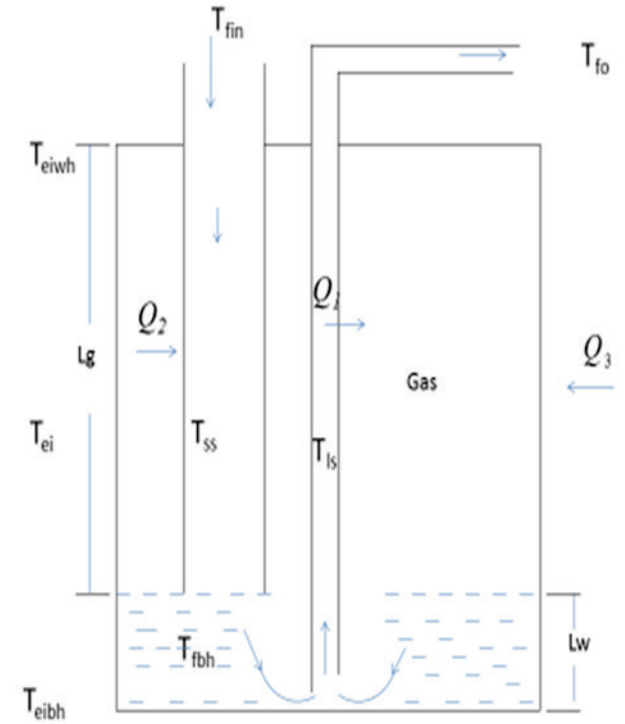
$$\frac{B'}{L_{R2}} \frac{d^2 T_{ls}}{dz^2} + B'' \frac{dT_{ls}}{dz} - T_{ls} + T_{ei} + D' = 0$$





# Boundary Conditions

- $T_{\text{water}}$  @ bottomhole same for annulus and the producing string;  
 $\left(\frac{dT_{ls}}{dz}\right)_{\text{bottomhole}} = 0$
- $T$  @ G-L interface same for gas & water



# Solution

$$T_{ss} = d_1 c_1 e^{\lambda_1 z} + d_2 c_2 e^{\lambda_2 z} + d_3 z + d_4$$

$$T_a = d_1 c_1 e^{\lambda_1 z} \left( 1 + \frac{w c_{pss} \lambda_1}{2 \pi r_{ss} U_{ss}} \right) + d_2 c_2 e^{\lambda_2 z} \left( 1 + \frac{w c_{pss} \lambda_2}{2 \pi r_{ss} U_{ss}} \right) + d_3 z + d_4 - \frac{w c_p}{2 \pi r_{ss} U_{ss}} \left( \phi_{ss} - \frac{g \sin \alpha}{c_{pss}} - d_3 \right)$$

$$T_{ls} = \alpha e^{\lambda_1 z} + \beta e^{\lambda_2 z} + g_G \sin \theta z + B'' g_G \sin \theta + T_{es} + D'$$

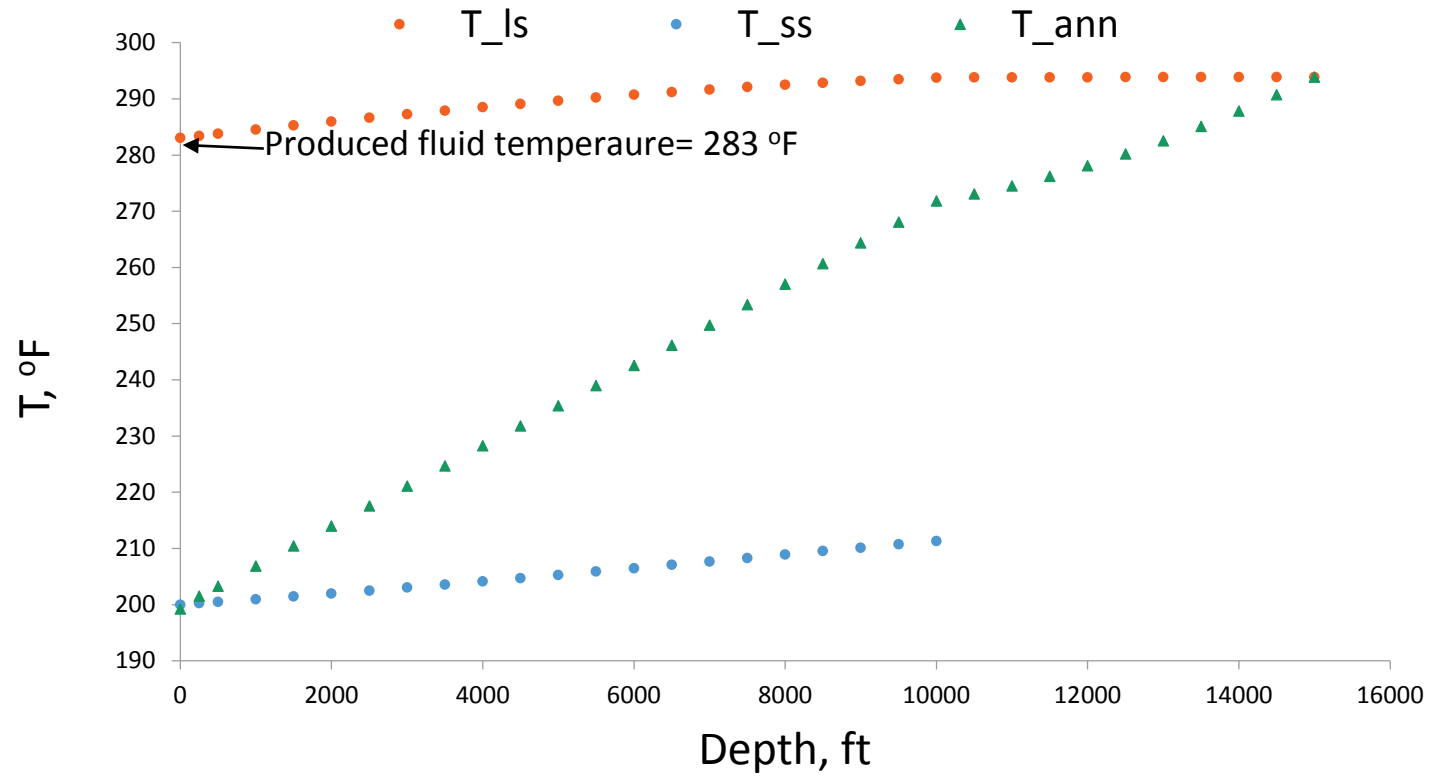
$$T_a = (1 - \lambda_1 B') \alpha e^{\lambda_1 z} + (1 - \lambda_2 B') \beta e^{\lambda_2 z} + g_G \sin \theta z + T_{es}$$



## Table 1: Base Case parameters

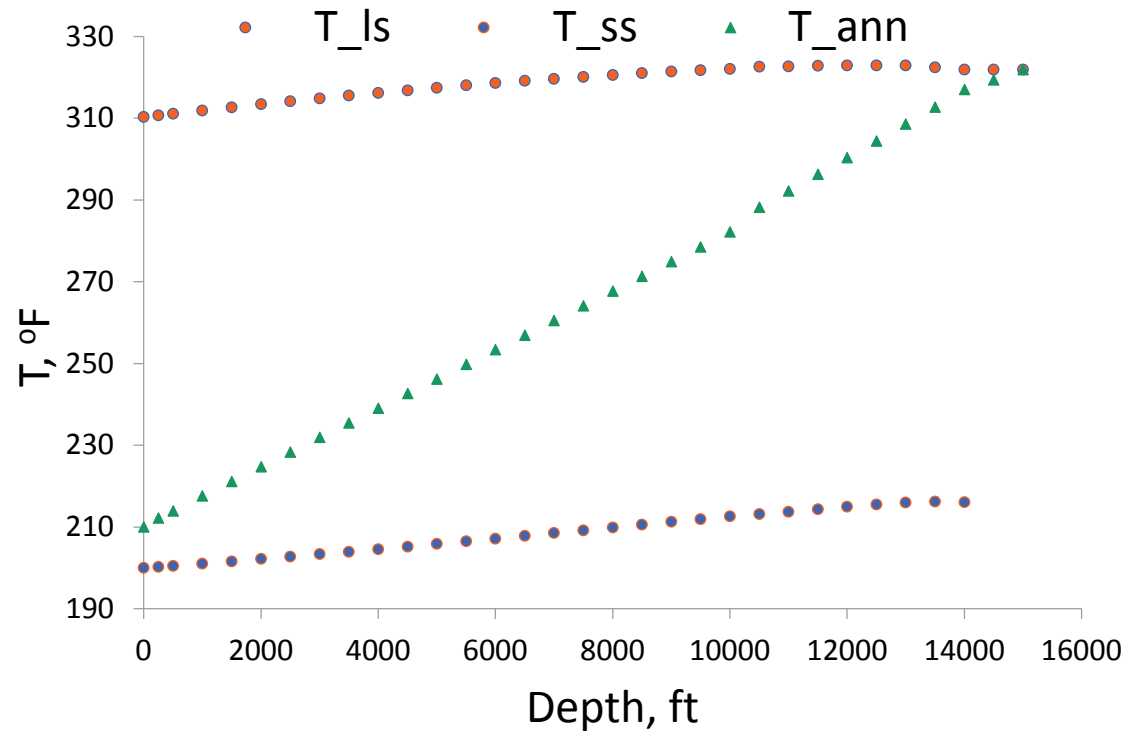
<b>Depths, ft</b>	<b>Total Well</b>	<b>15,000</b>	<b>Temperatures °F</b>	<b>Formation top</b>	<b>75.0</b>	
	N <sub>2</sub>	10,000				
<b>Diameters, in</b>	Casing (inner)	17.0			Formation bottom	450.0
	Casing (outer)	18.5				
	Cement (Outer)	25.0				
	Prod tube (Inner)	3.0			Injection Fluid, top	200.0
	Prod tube (Outer)	3.5				
	Injection tube (Inner)	8.0				
	Injection tube (Outer)	9.0		Produced Fluid, top	283.02	
<b>Conductivities Btu/hr-ft-°F</b>	Tubing & Casing	26.0				
	Cement	1.0	<b>Production Rate, gpm</b>		1,000	
	Formation	1.4	<b>Insulation thickness, inch</b>		0.5	
	Insulation	0.02				





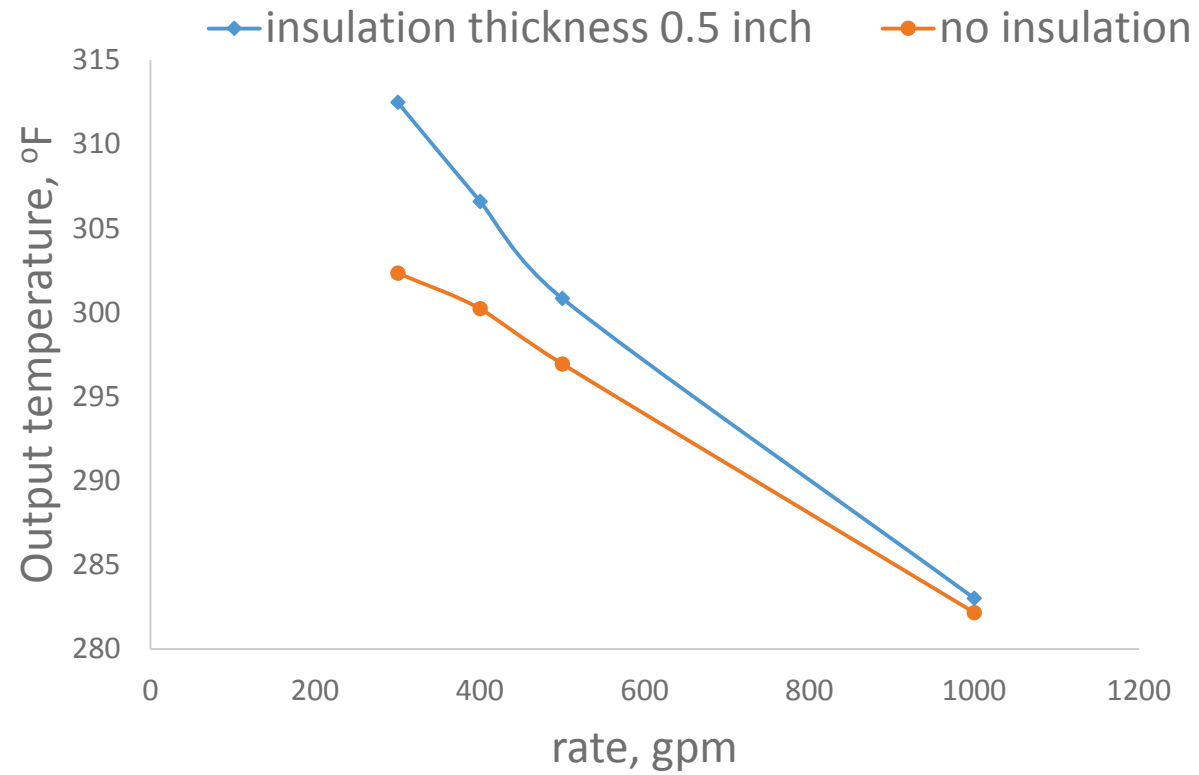
**Fig: Fluid temperature in three conduits (q=1000 gpm and insulation 0.5 inch)**





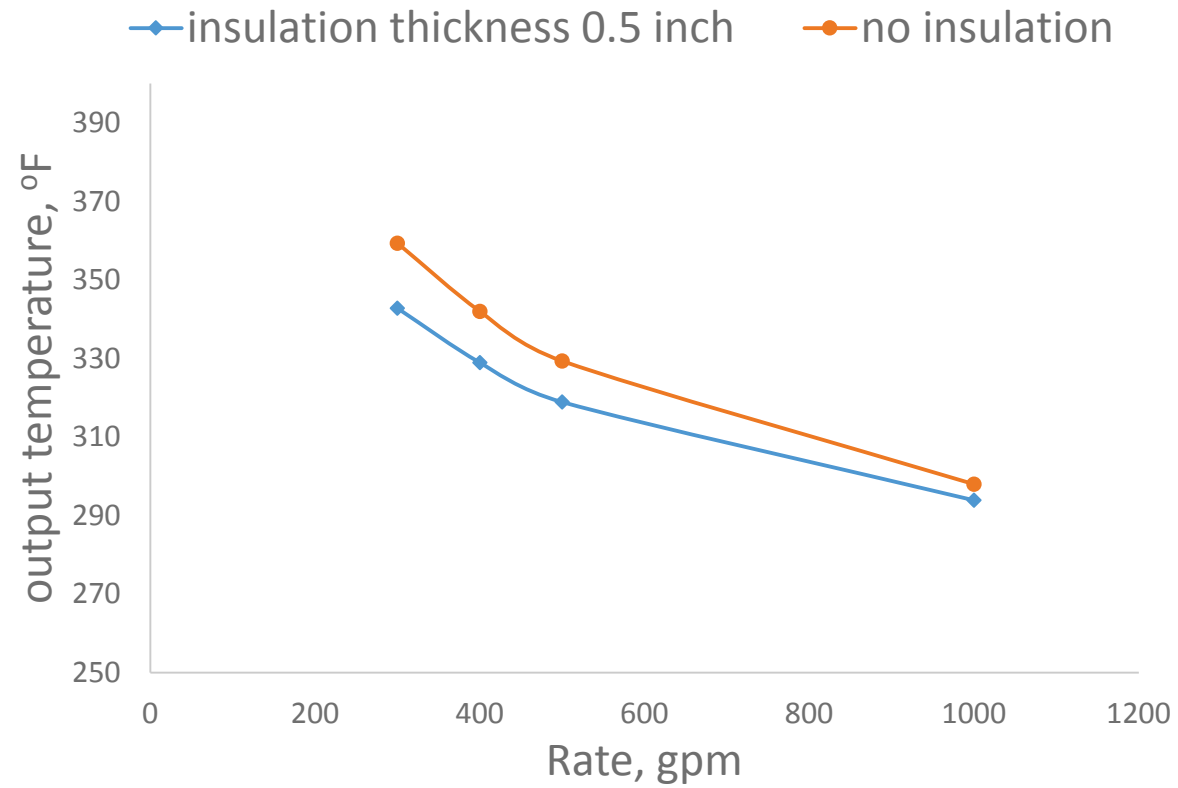
**Fig. Fluid temperature in three conduits at  $q=1000$  gpm and  $N_2$  depth=14000 ft**





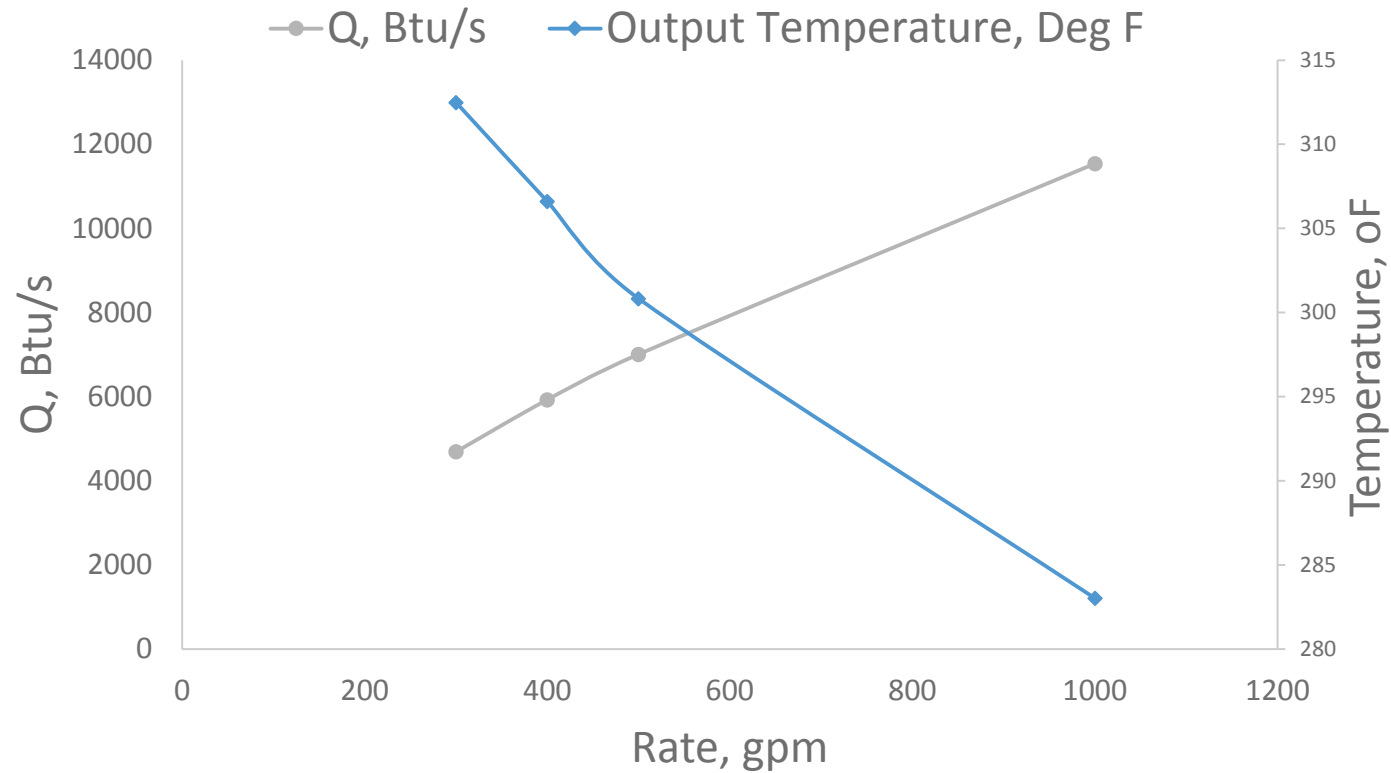
**Fig: Production temperature at the surface**





**Fig: Bottomhole Temperature with different rates**





**Fig: Power and Output Temperature with different rates**





# Conclusion

- At all flowrates, increasing the Nitrogen coverage increases fluid temperature at the wellhead
- The inclination of Tann curve changes as we move from a gas filled annulus to a water filled one
- As production rate increases, Temperature rise decreases for both insulated and uninsulated cases

